

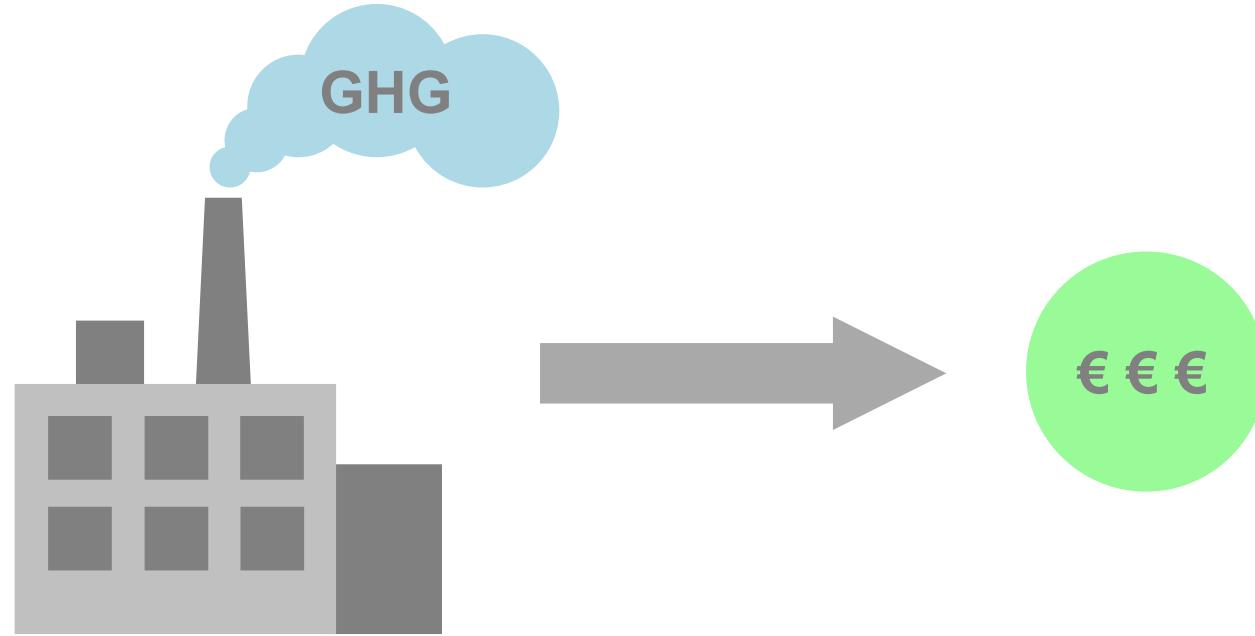
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# Chemical Models and Energy Balance for Optimal Gas Utilisation

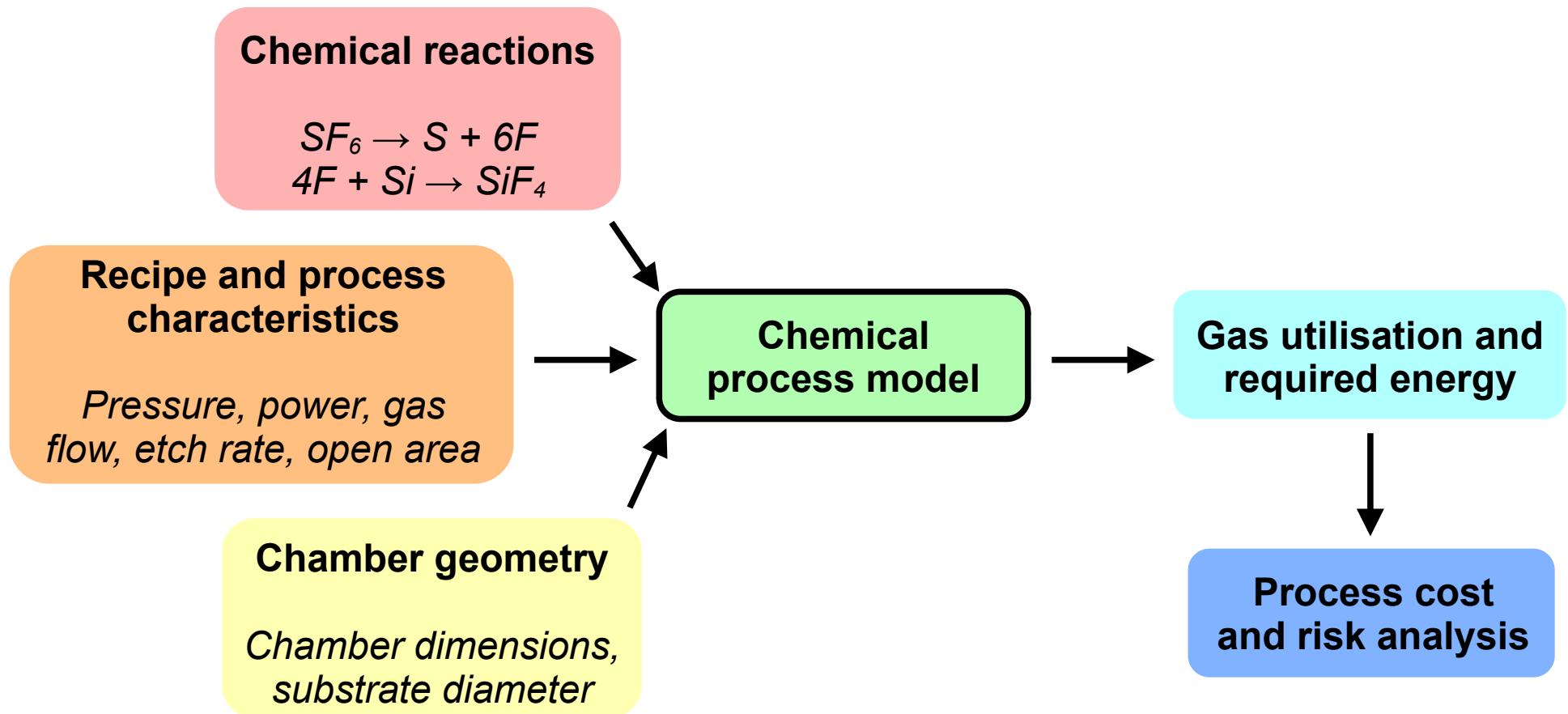
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- » Motivation
- » Chemical Process Model
- » Advanced Process Model
- » Process Cost and Risk Analysis
- » Summary

- » Semiconductor fabs must reduce greenhouse-gas emissions while maintaining performance.



- » Chemical process models help us optimise gas usage while maintaining process stability.



# Chemical Process Model: Example

Reaction:

Si etch with SF<sub>6</sub>



Dissociation of SF<sub>6</sub>

Process:

Demo,Trench:ResistMask:1%

800 sccm, 3.5kW, Si etch

{5299.65, 0.01}

{3.325, 3500}

800



DRIE recipe  
(Etch rate of the  
Si-etch step only)

ER / Depo rate [nm/min], Open area =

$p_{\text{Chamber}}$  [Pa],  $P_{\text{source}}$  [W] =

Inward flux of process gas SF6 [sccm] =

Chamber:

Substrate diameter [mm] =

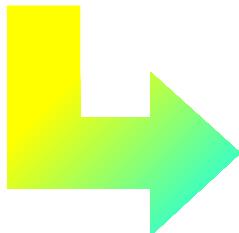
SPTS Rapier 200 mm

200.



Chamber dimensions

Amount of  
radicals  
consumed

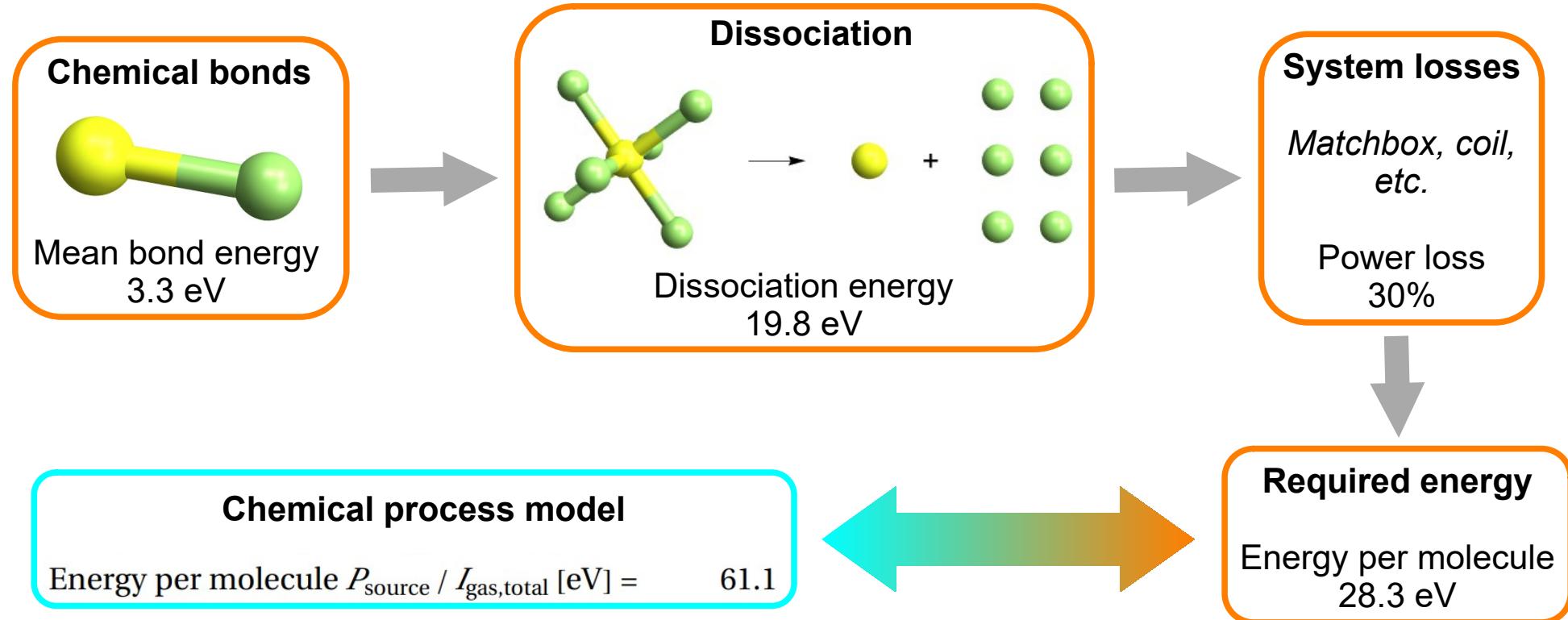


Process gas flux directly used SF6 [sccm] = 2.08  
Utilization factor process gas SF6 [%] = 0.26  
Energy per molecule  $P_{\text{source}} / I_{\text{gas, total}}$  [eV] = 61.1

# Chemical Process Model: Energy for Dissociation

6

- Source power determines the degree to which the process gas dissociates.



- Only a fraction of incoming gas actually reacts on the wafer.

## Small open area

ER / Depo rate [nm/min], Open area = {5299.65, 0.01}

$p_{\text{Chamber}}$  [Pa],  $P_{\text{source}}$  [W] = {3.325, 3500}

Inward flux of process gas SF6 [sccm] = 800

## Large open area

ER / Depo rate [nm/min], Open area = {16 224.5, 0.68}

$p_{\text{Chamber}}$  [Pa],  $P_{\text{source}}$  [W] = {3.325, 3500}

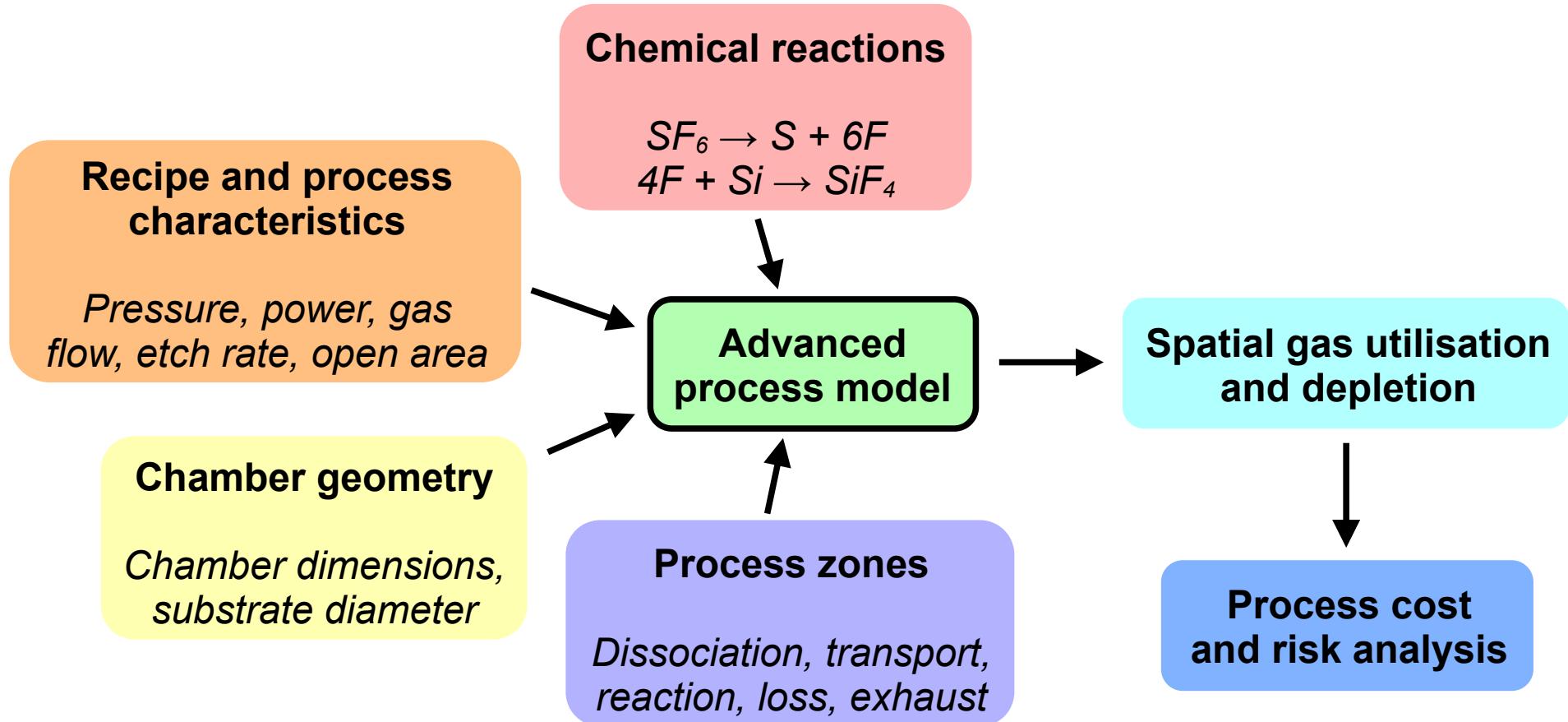
Inward flux of process gas SF6 [sccm] = 800

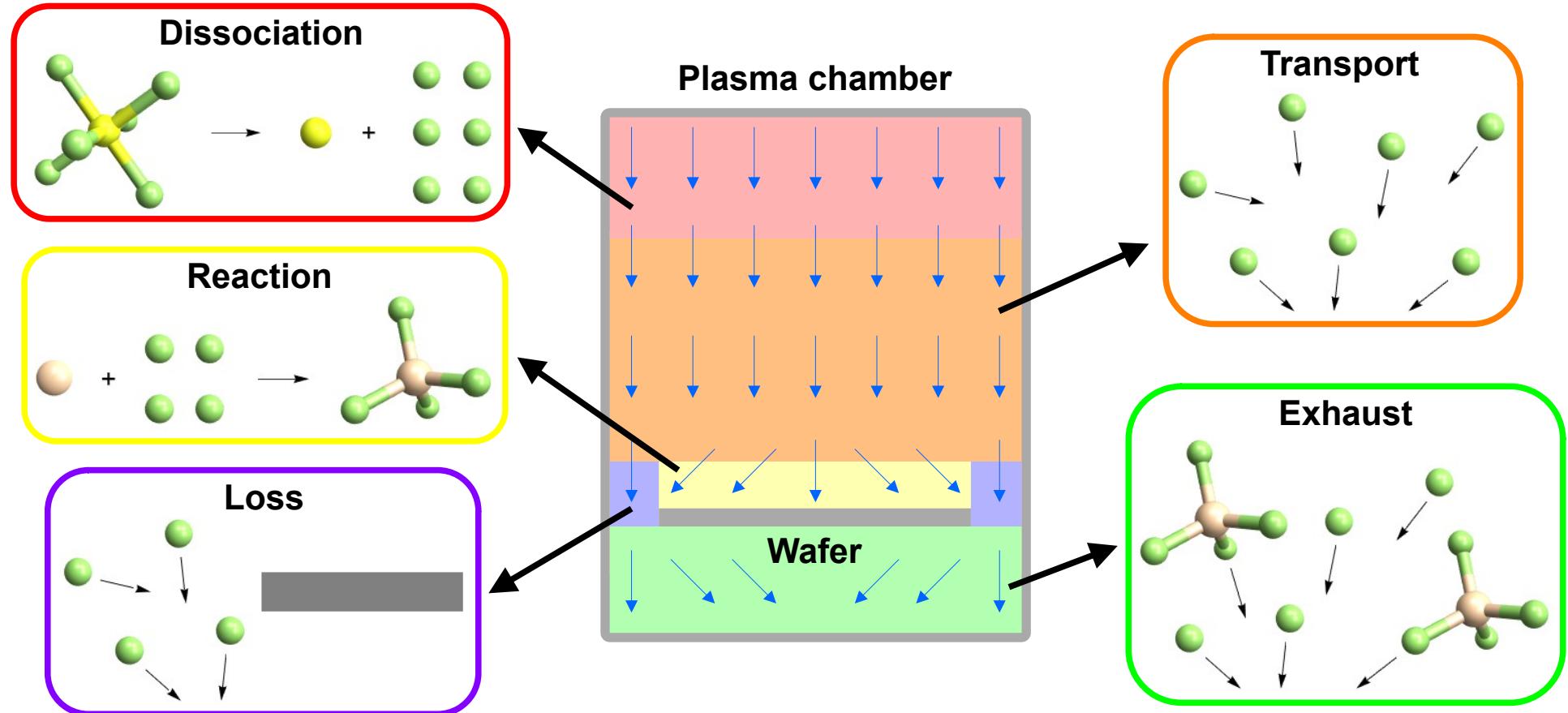
Process gas flux directly used SF6 [sccm] = 2.08  
Utilization factor process gas SF6 [%] = 0.26

Process gas flux directly used SF6 [sccm] = 432.  
Utilization factor process gas SF6 [%] = 54.

Radicals are oversupplied  
Surface-reaction-controlled process

Radicals are depleted  
Transport-controlled process



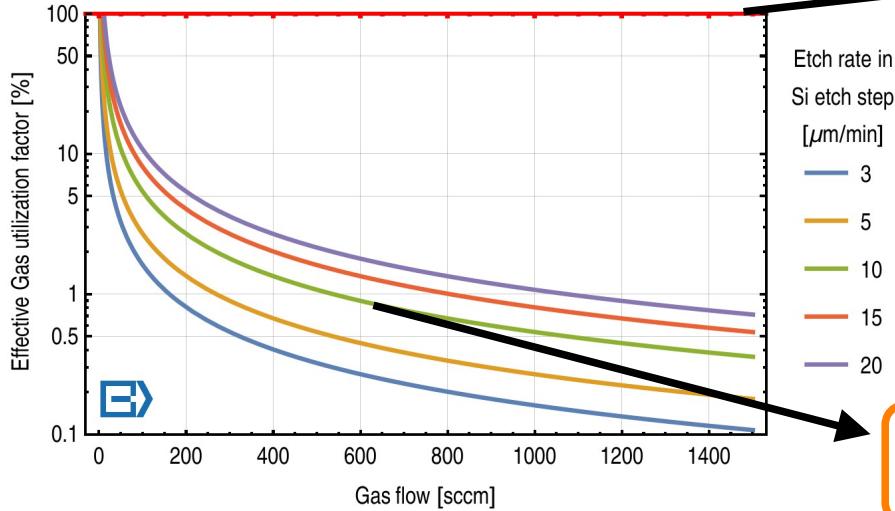


# Advanced Process Model: Example

10

- The graph shows how gas utilisation and etch rate depend on gas flow.

Chamber: SPTS Rapier 200 mm, reaction: Si etch with SF<sub>6</sub>,  
gas usage: 73%, open area: 1%.



**Utilisation limit**  
*Theoretical maximum*

Perfect gas utilisation,  
operation below the limit

**Flat region**  
Surface-reaction-controlled regime

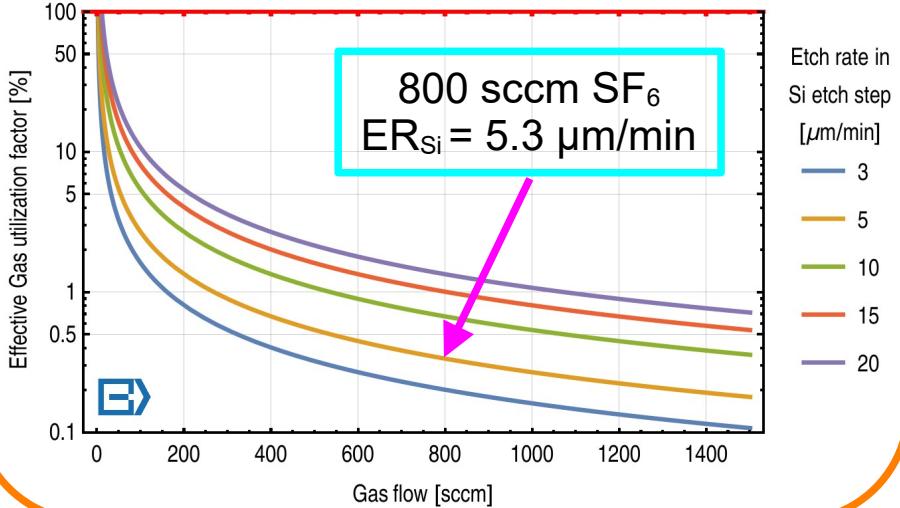
**Utilisation curve slope**  
*Regime indicator*

**Transition region**  
Efficient operating regime

**Steep region**  
Transport-controlled regime

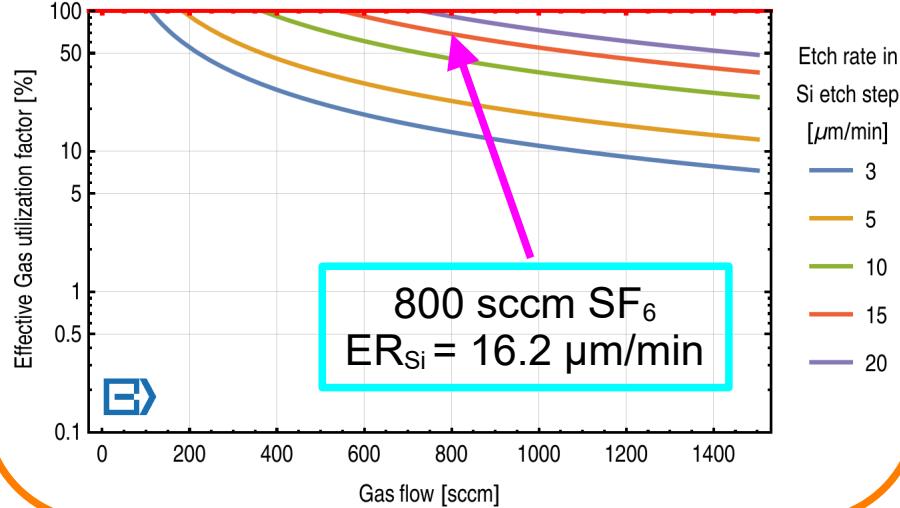
## Small open area

Chamber: SPTS Rapier 200 mm, reaction: Si etch with  $\text{SF}_6$ ,  
gas usage: 73%, open area: 1%.



## Large open area

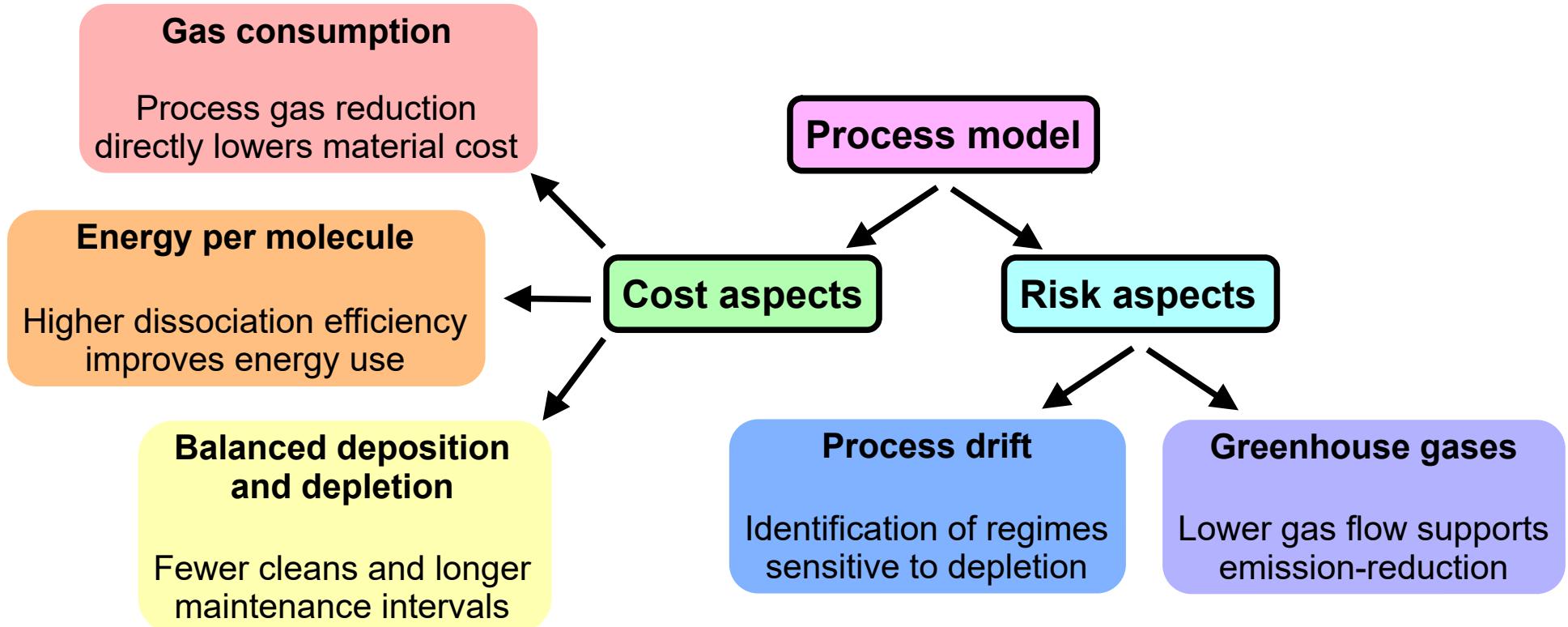
Chamber: SPTS Rapier 200 mm, reaction: Si etch with  $\text{SF}_6$ ,  
gas usage: 73%, open area: 68%.



Surface-reaction-controlled process

Transport-controlled process

- » The process models link gas utilisation directly to cost and risk.



- ☒ The chemical process model links recipe parameters, chamber geometry, and reaction chemistry to predict gas utilisation and energy efficiency.
- ☒ The advanced process model adds spatial zones and transport effects, identifying oversupply and depletion regimes.
- ☒ These models explain the opposite behaviour observed for small and large open areas.
  - Small → surface-reaction-controlled, oversupply
  - Large → transport-controlled, depletion
- ☒ The model results show that gas flow can be reduced without reducing etch rate, lowering both process cost and greenhouse-gas emissions.

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Thank you for your attention.

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